

DUPIC

Fission Product Behaviors in Spent Fuel Materials
during DUPIC Fuel Fabrication Process

150

DUPIC

(IMEF) M6

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, OREOX(.)

Cs - 137

99%

, Zr - 95 Ru - 103

Abstract

In order to obtain the fundamental data for the analysis of fission product behaviors during DUPIC fuel fabrication process, which is to convert spent PWR fuel into CANDU reactor fuel, the measurement system of radioactivity in spent fuel materials by gamma spectrometry technique was installed in IMEF M6 hot cell, and the preliminary analysis on the release behaviors of fission gas during the DUPIC fuel fabrication process were conducted. Based on the radioactivity measurement for the spent oxidized powder, green pellet and the sintered pellet produced from DUPIC fabrication process, it was found that little Cs - 137 was released during OREOX process, but almost 99% of Cs - 137 was released during sintering process. The release rate of both Zr - 95 and Ru - 103 was not so high during sintering process.

1.

DUPIC(Direct Use of spent PWR fuel in CANDU reactors)
CANDU

가 . DUPIC
UO₂ fragments
OREOX(Oxidation and Reduction of Oxide Fuel)

DUPIC Table 1
OREOX Table 1 450 ~ 700
3 1,800 [1~2].
(I - 129, Kr -
85) (Cs - 134, 137)

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ORNL[3] CEA[4], AECL[5~7] AEAT[8]

(source term) . Table 2

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2.

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3.21 wt. %, 27,300 MWD/MTU, 15 (1
) : 1986. 10) G23 A1, B5, B7, C8, D9 (G23 - 5B
) . 5 UO₂ fragments 450

Table 1

OEROXed

(green pellet)

̃-spectrometry system

Table 1. Optimal operating conditions for DUPIC fuel fabrication

| Process | Operating conditions |
|----------------------------------|--|
| OREOX - 3 Cycles | <ul style="list-style-type: none"> ■ Oxidation condition - 450°C, 2 hrs, Air, 5.5 L/min ■ Reduction condition - 700°C, 7 hrs, Ar/4% H₂, 13 L/min ■ Passivation condition - 80°C, 4 hrs, Ar/2% O₂, 2 L/min |
| Milling | - Attrition Ball - milling, 20 min, 450 & 600 rpm |
| Pre - compaction and Granulation | - Precompaction : 0.8 ton/cm ² - Granulation : Sieve # 12 pass(1mm) |
| Mixing | - 0.2 wt% zinc stearate add, 20 min - mixing |
| Final compaction | - Pressure : 1.2 ~ 1.8 ton/cm ² |
| Dewaxing | - 800°C, 3 hrs, Ar/4% H ₂ , 4 L/min |
| Sintering | - 1,800°C, 10 hrs, Ar/4% H ₂ , 8 L/min |

Table 2. Release rate of fission products on the experiments conducted in various countries

| | ORNL (USA) | CEA (France) | CRL (AECL) | AEAT (UK) |
|-------------------------|---|--|---|---|
| Cs - 137 | 63 ~ 100% | 15 ~ 68% | 75 ~ 100% | 40%(1673K) 1 ~ 2%(1273K) |
| Ru - 106 | < 5% | < 5% | ~ 2 % | - |
| Eu - 154 | 14 ~ 57% | < 15% | - | - |
| Zr - 95 | - | - | <2 %(2,273K) | - |
| Experimental conditions | - UO ₂ fragment - 2000~2440K - Steam, H ₂ , Air | - Burn up : 19940~ 36700 - 1900~2370K - Steam, H ₂ | - UO ₂ fragment - Burn up : 10700~ 22700 - 1625~2350K - Steam, Air | - UO ₂ fragment - Burn up : 26000 - 923~1673K - Air |

(IMEF) M6

Fig. 1

가

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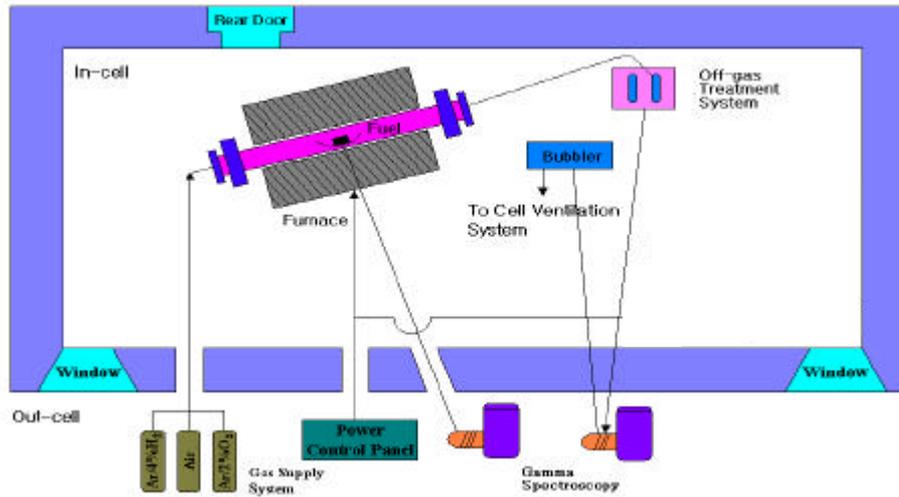


Fig. 1. Schematic diagram of experimental apparatus for the analysis of fission product behaviors during DUPIC fuel fabrication process.

line : OEROXed on -

가 450 , 700 1,800

가 : TGT(Thermal Gradient Tube), HEPA filter, Balston filter, Bubbler

가 : () 가

(2),

3.

3.1 OREOX

OREOX

G23 - 5B

()

ORIGEN

Table 3

Table 3

Cs - 137

28%

, Kr - 85

Eu - 154

, I -

129 Xe - 133

Table 3. Fission product activity in oxidized powder (G23 - 5B powder)

| Nuclide | g/MTHM | Ci/MTHM | Contribution to total F/P activity, % |
|-----------|------------------------|------------------------|---------------------------------------|
| Cs - 134 | 4.96×10^{-1} | $6.42 \times 10^{+2}$ | 0.30 |
| Cs - 137 | $6.88 \times 10^{+2}$ | $5.99 \times 10^{+4}$ | 28.15 |
| Ru - 106 | 3.34×10^{-3} | $1.12 \times 10^{+1}$ | 0.01 |
| Ce - 144 | 3.73×10^{-4} | 1.19×10^0 | 0.00 |
| Eu - 154 | 6.64×10^0 | $1.79 \times 10^{+3}$ | 0.84 |
| Eu - 155 | 1.05×10^0 | $4.87 \times 10^{+2}$ | 0.23 |
| Sr - 90 | $3.35 \times 10^{+2}$ | $4.36 \times 10^{+4}$ | 20.49 |
| Nb - 95 | 2.68×10^{-21} | 3.81×10^{-20} | 0.00 |
| Zr - 95 | 2.19×10^{-21} | 1.72×10^{-20} | 0.00 |
| Tc - 99 | 4.96×10^{-1} | $1.11 \times 10^{+1}$ | 0.01 |
| Rh - 106 | 3.14×10^{-9} | $1.12 \times 10^{+1}$ | 0.01 |
| Sb - 125 | 2.29×10^{-1} | $2.37 \times 10^{+2}$ | 0.11 |
| H - 3 | 1.92×10^{-2} | $1.85 \times 10^{+2}$ | 0.09 |
| C - 14 | 2.17×10^{-5} | 9.68×10^{-5} | 0.00 |
| Kr - 85 | 7.50×10^0 | $2.94 \times 10^{+3}$ | 1.38 |
| I - 129 | $1.45 \times 10^{+2}$ | 2.55×10^{-2} | 0.00 |
| I - 131 | 0.00×10^0 | 0.00×10^0 | 0.00 |
| Xe - 133 | 0.00×10^0 | 0.00×10^0 | 0.00 |
| Total F/P | 2.81×10^4 | 2.13×10^5 | |

Table 1

, OREOX

450 ,

5.5 L/min

2 ,

700 , (4% H₂ + 96% Ar) 가

13 L/min

7 ,

4 /min

3

OREOX

Fig. 2

Eu - 154, Eu - 154 normalization, 8.8 OREOX, OREOX, OREOX, AECL, DUPIC, OREOX, Kr - 85 (), Cs - 137, [9].

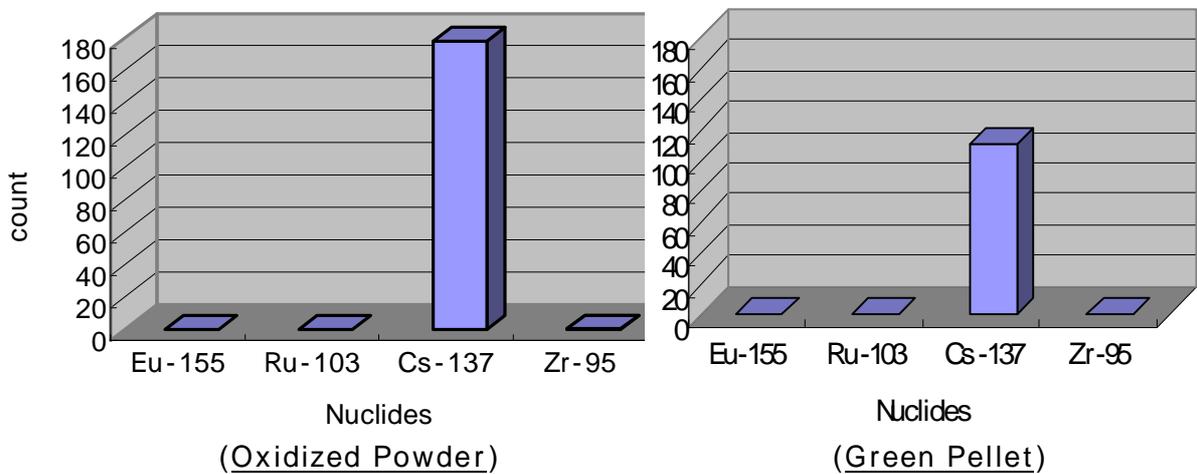


Fig. 2. Count number of various fission products in the oxidized powder(before OREOX) and green pellet(after OREOX).

3.2

Table 1 (4% H₂ + 96% Ar), 5 /min, 1,800, 10, Fig. 2, Eu - 154, normalization, Cs - 137, Ru - 103, DUPIC, DUPIC, Fig. 3.

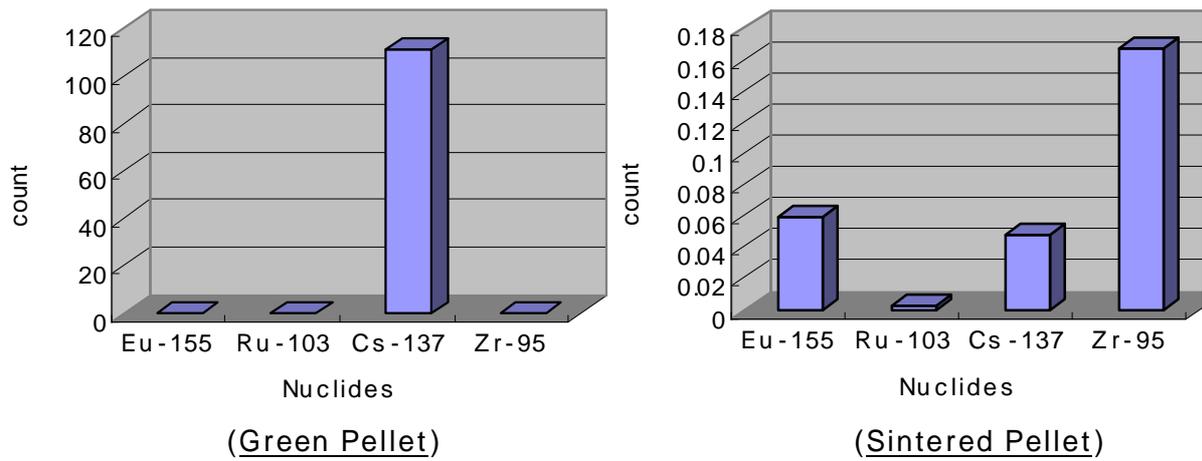


Fig. 3. Count number of various fission products the in green pellet(before sintering) and sintered pellet(after sintering process).

3.3

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OREOX

가

Fig. 4

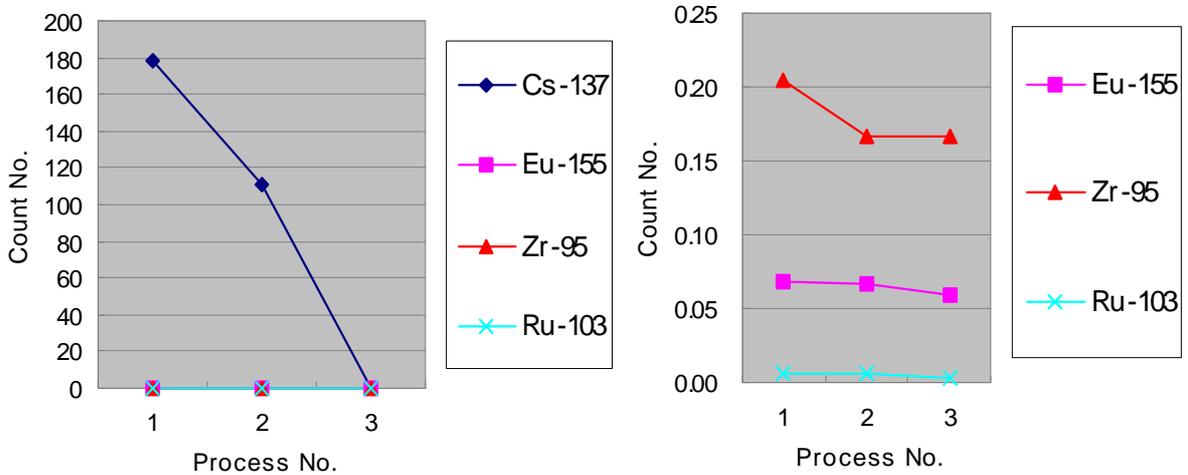


Fig. 4. Count rates of fission products during DUPIC fuel fabrication process [1 : Before OREOX process, 2 : After OREOX, 3 : After Sintering process].

15% OREOX , Cs - 137 99%

DUPIC Ru - 103, Zr - 95

4.

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■ DUPIC

OREOX

Cs - 137

■ Cs - 137 99% , Zr - 95 Ru - 103

■ Cs - 137 DUPIC

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