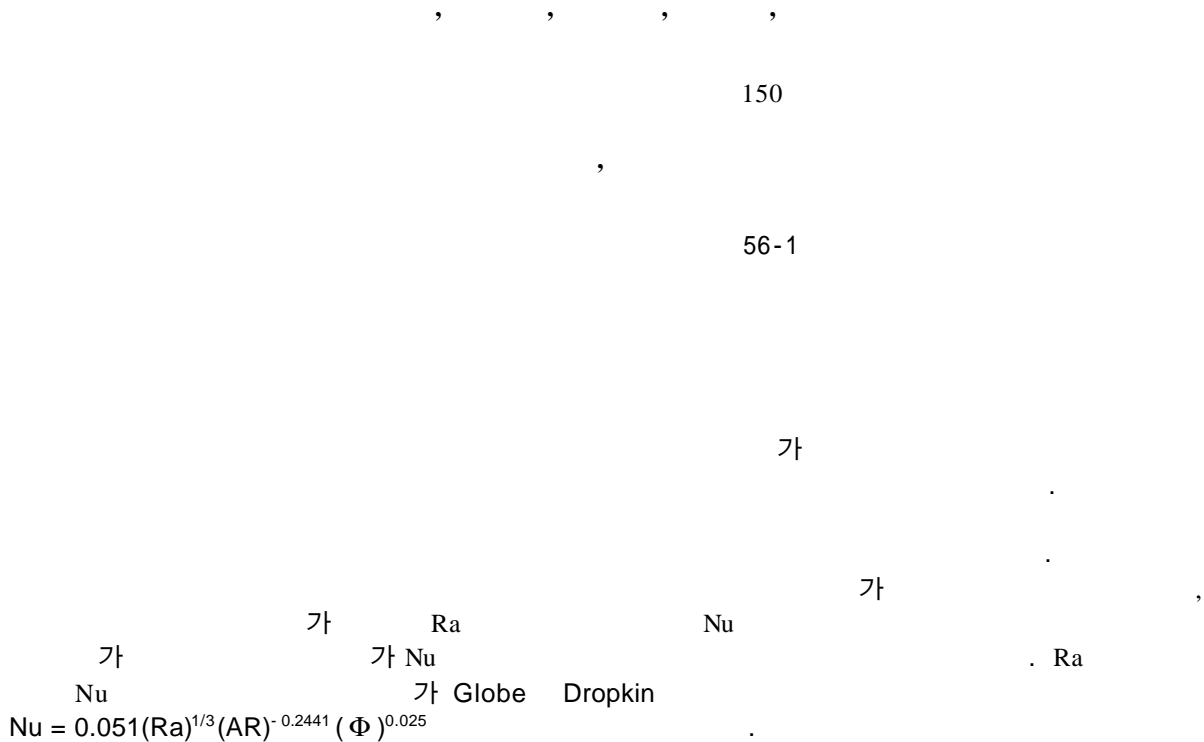


Correlation Development of Natural Convection Heat Transfer in Consideration of Aspect Ratio Change and Coolant Boiling



Abstract

A new correlation on natural convection heat transfer with crust formation in the molten metal pool has been developed in consideration of coolant boiling effect and of aspect ratio change by an increase in crust thickness. Two test results of the convection cooling case, natural and forced convection cooling cases, and of the boiling case were used in the present study. The experimental results have shown that the Nusselt number of the case with boiling condition in the molten metal pool is greater than that of the case with non-boiling condition at the same Rayleigh number. Even though the Rayleigh number rapidly decreases due to an increase of the crust thickness, the Nusselt number does not rapidly decrease because of the aspect ratio effect. From the experimental results, the new correlation between the Nusselt number and Rayleigh number in the molten metal pool with the crust formation has been developed as $Nu = 0.051(Ra)^{1/3}(AR)^{-0.2441}(\Phi)^{0.025}$ using Globe and Dropkin correlation.

1.

가
plenum, (cavity)

ZrO₂ 가 1 가 (UO₂)
Zircaloy
(decay heat)

가 Rayleigh-Benard 가
pool
(conducting thermal barrier) [1, 2, 3].

가 가
(Molten Core Concrete Interaction and Debris Coolability)
[4, 5, 6]가

microscopic
(late phase melt progression)
pool
가

Pr 가 1 가 pool 가
가 (aspect ratio)가 가
가 가

Rayleigh-Benard Nu Ra, Pr, (aspect ratio)
Ra 가 가, Pr 가
가, 가 Nu 가 [7, 8, 9, 10]. 가

Ra Nu 가
가 Nu
2 가

가 Pr 가 1 가 가 1/6

4/5

가

가

가

가

2.

(cavity)

가 1/6 4/5

가 100

Pr 가 1

가 eutectic

가 Bi가 50 %, Pb가 27 %, Sn 13 %, Cd가

10%

가 70

3

11

가

가 232°C

(Tin)

가

digital

가

4가

12

1

3.

11 12

가

Rayleigh-

Benard

가

[13-17].

$$Nu = a Ra^b \quad (1)$$

Nu , Ra
 2가 .
 Globe Dropkin Rossby Pr 가 1 Ra ,
 Pr , Ra 가 가 , Pr 가 가 , 가
 Nu 가 .
 가 Ra 가 Nu 가 가
 가 .
 가 ,
 가 가 가
 5 Ra 가 Nu 가
 가 .
 Ra 가 가 Nu 가 가 , Pr 가 1
 Globe Dropkin Rossby
 . Pr 가 0.017
 Pr 가 0.024 Globe Dropkin Rossby
 Rossby 8 % , 15 %
 Nu 가 Globe
 Dropkin
 6 Ra 가 Nu Globe Dropkin 가
 .
 Globe Dropkin
 11 % , 17 %
 Nu 가
 .
 7 Ra 가 Nu Globe Dropkin
 가 가
 Globe Dropkin .

20 %,

30 %

21 %,

31 %

가

가

가

가

Nu 가

가

가

가 Ra 가

Globe Dropkin

$$Nu = 0.051(Ra)^{1/3}AR^e \quad (2)$$

- 가 : $e = -0.0736$ ($0.086 < AR < 0.167$)

- 가 : $e = -0.2441$ ($0.369 < AR < 0.759$)

Pr 가

Pr 가

Nu

$$Nu \propto Pr^{0.074}$$

가

Globe Dropkin

, Pr 가

Globe Dropkin

가 Nu

Pr Globe Dropkin

Pr

Pr 가

가

8

Nu 가

가

가

가

가

$$Nu = 0.051(Ra)^{1/3}(AR)^{-0.2441} \Phi^n \quad (3)$$

(3)

Φ^n

Φ

가

(3)

n

가

, n 0.025

$$Nu = 0.051(Ra)^{1/3}(AR)^{-0.2441}(\Phi)^{0.025} \quad (4)$$

Pr 가 가

4.

- Globe Dropkin
가 가
- Ra Nu
가 Nu 가 Nu 가

- Nu 가
Globe Dropkin Nu 가
- Ra Nu 가 가 Globe Dropkin

Nu =

$$0.051(Ra)^{1/3}(AR)^{0.2441}(\Phi)^{0.025}$$

- 가 가

- a :
- AR : (= l/c)
- b :
- c : 가 , m
- c_p : , J/(kg.K)
- d : , m
- e :
- g : 가 , m/s²
- h : , W/(m²K)
- k : , W/(mK)
- l : (= d-t), m
- n :
- Nu : Nusselt (= hl/k)
- Pr : Prandtl (= /)
- Ra : Rayleigh (= g Δ T l³ / ())

t : , m
 T : ,
 T_b : ,
 T_c : ,
 T_s : 가 ,
 ΔT : . ,

α : $(= k / (\rho c_p))$, m²/s
 β : , 1/K
 ν : , m²/s
 ρ : , kg/m³
 Φ : $((T_b - T_c) / (T_s - T_c))$

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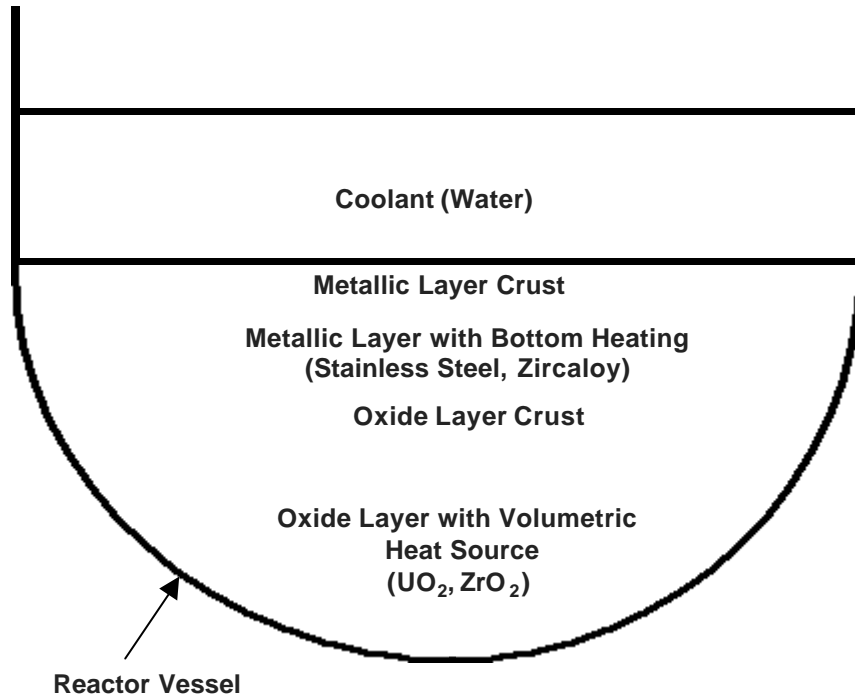
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1.

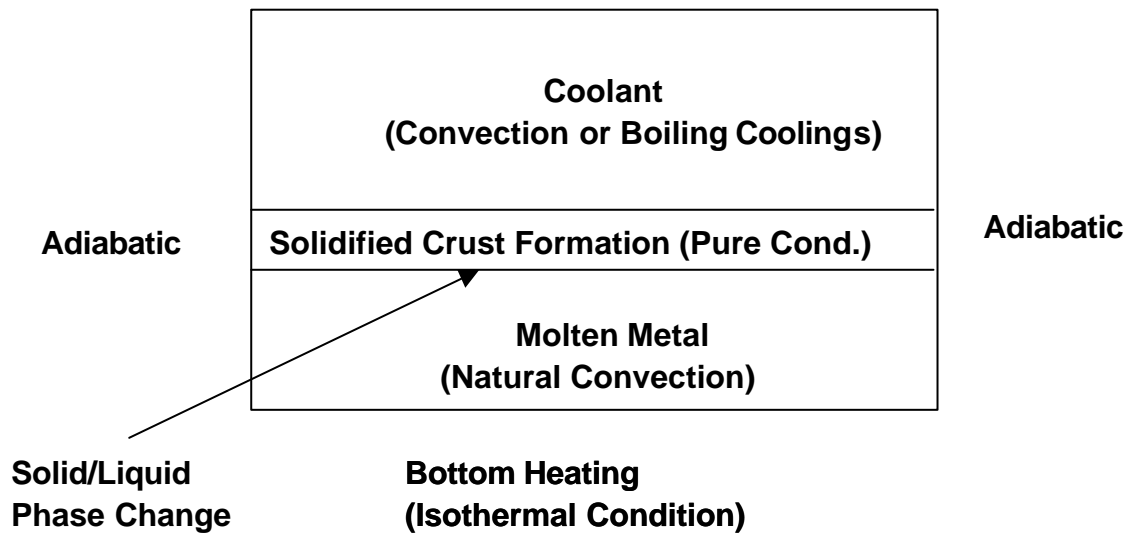
	Natural Convection Case		Boiling Case
	Low Aspect Ratio Case	High Aspect Ratio Case	
Test Section Geometry (X x Y x Z)	450 x 150 x 150 (mm x mm x mm)	250 x 150 x 350 (mm x mm x mm)	250 x 250 x 350 (mm x mm x mm)
Height of the metal layer	75 (mm)	200 (mm)	200 (mm)
Height of the coolant layer	75 (mm)	150 (mm)	150 (mm)
Metal material	Wood' s metal	Wood' s metal	Tin
Coolant material	Water	Water	Water
Ra range in the metal pool	$10^4 - 10^6$	$10^5 - 10^7$	$10^6 - 10^8$
Teflon bar locations	(X/2, Y/2), (3/4X, Y/2)	(X/4, Y/2), (X/2, Y/2), (3/4X, Y/2)	(X/4, Y/2), (X/2, Y/2), (3/4X, Y/2)
Heater capacity	3 (kW)	4 (kW)	19.8 (kW)

2. 가

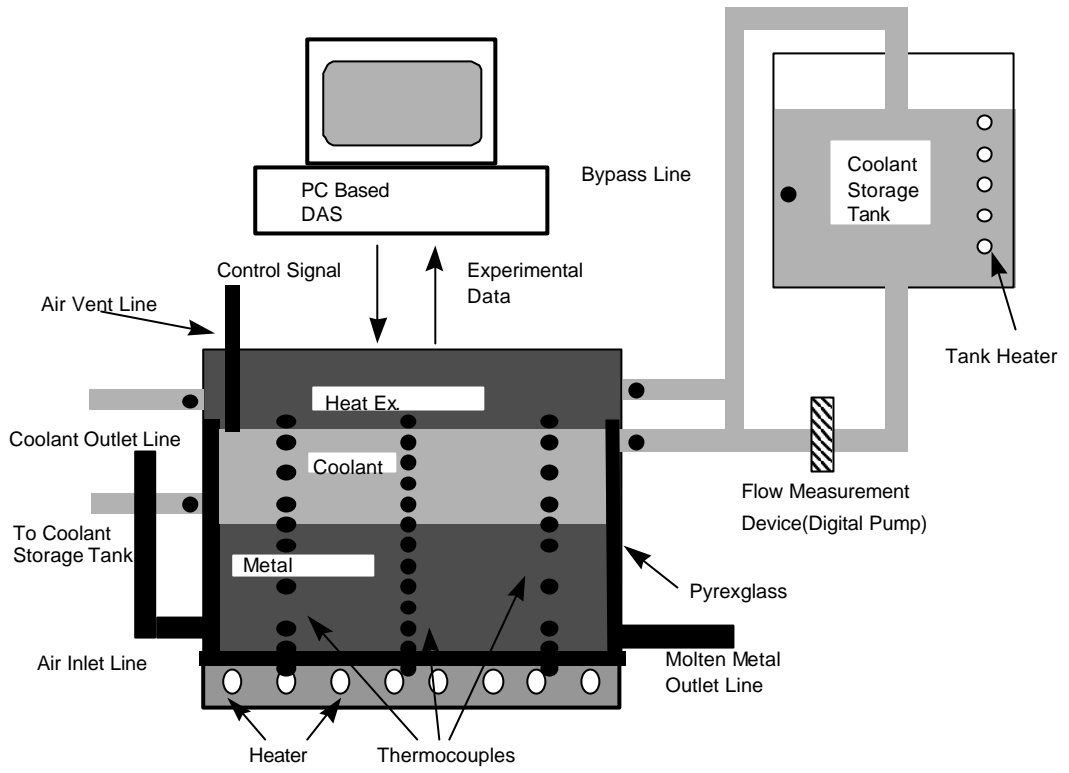
	Working Fluid	a	b	Ra Range	Pr
Globe & Dropkin	Mercury	0.051	1/3	$1.51 \times 10^5 < Ra < 6.76 \times 10^8$	0.022
Rossby	Mercury	0.147	0.247	$2.0 \times 10^4 < Ra < 5.0 \times 10^5$	0.024
Threlfall	Gas Helium	0.173	0.280	$4.0 \times 10^5 < Ra < 2.0 \times 10^6$	0.8
Heslot et al.	Gas Helium	0.096	0.353	$3.0 \times 10^5 < Ra < 4.0 \times 10^7$	0.8
Chu & Goldstein	Water	0.183	0.278	$2.76 \times 10^5 < Ra < 1.05 \times 10^8$	6



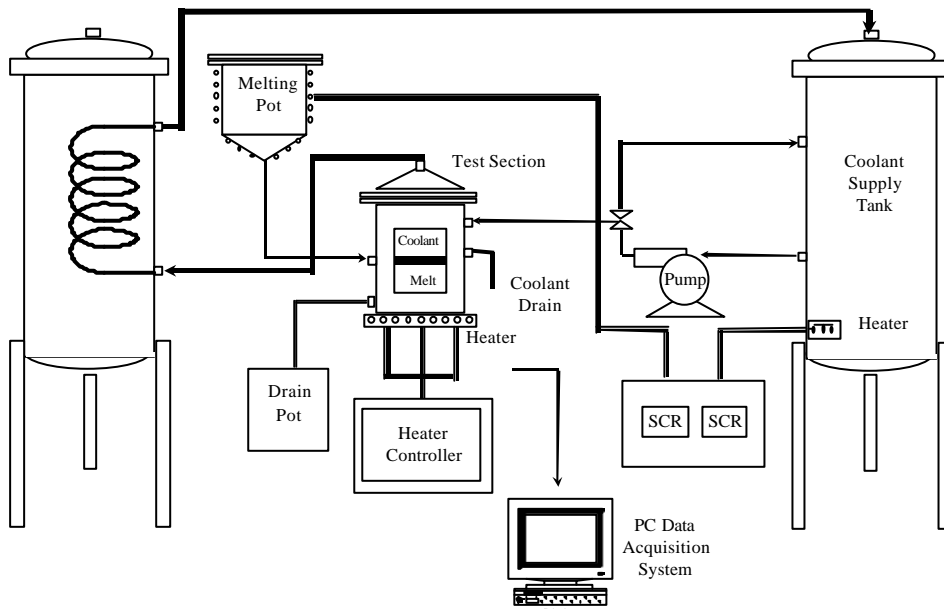
1.



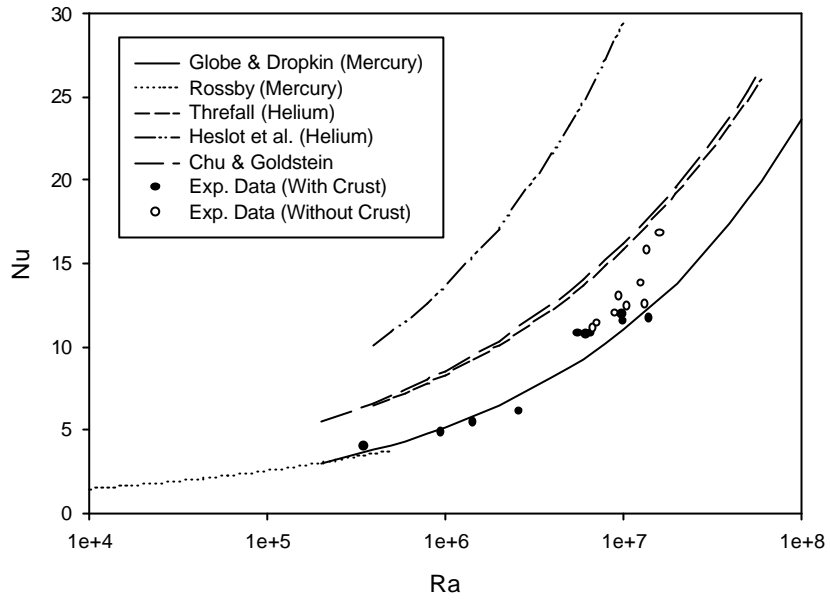
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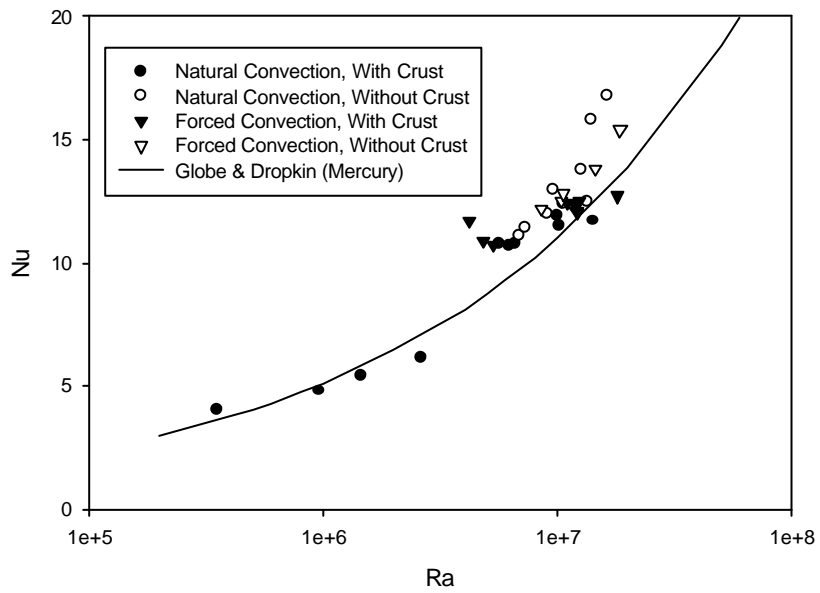
3. 가



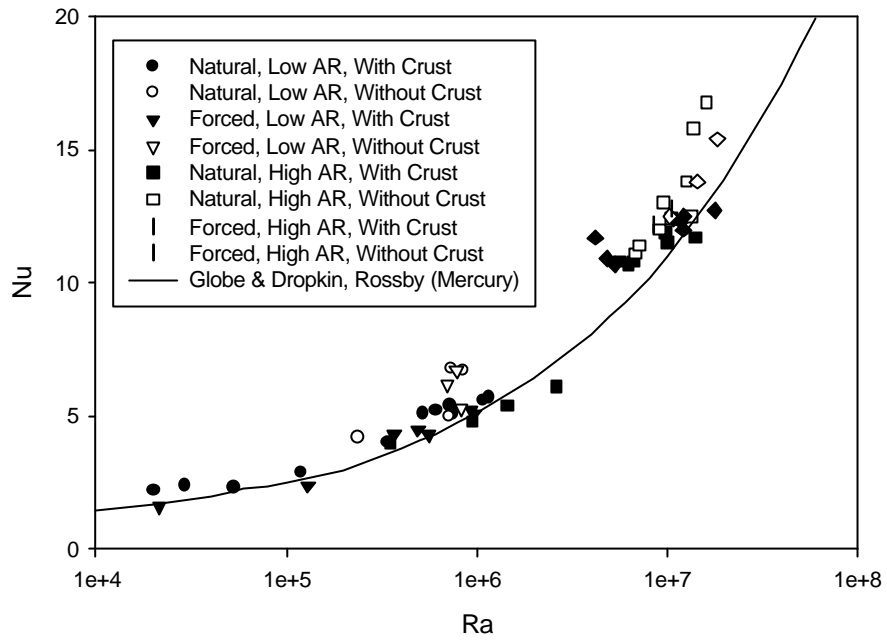
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5. 가

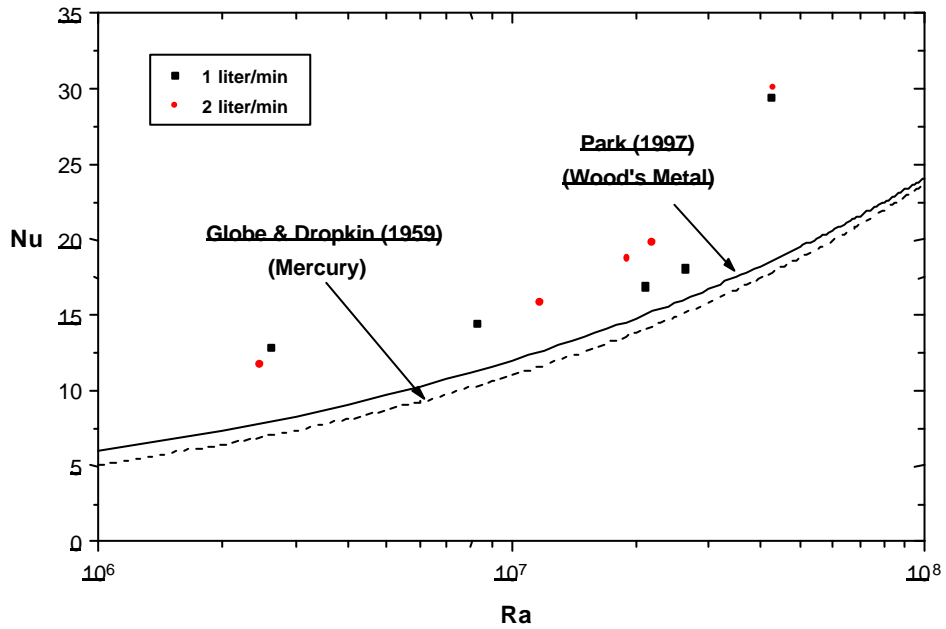


6. 가



7. 가

Globe & Dropkin



8.