

Conceptual Design of the Primary Cooling System Pump in Consideration of the Variable Flow Rate in the Research Reactor

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1. Introduction

Primary Cooling System (PCS) pump circulates the coolant in order to remove the heat generated from the reactor core in the research reactor. Typical PCS consists of two parallel 50% capacity pumps for safety as shown in Fig. 1. When one pump stops abnormally, the other is continuously operating to circulate the coolant. If two PCS pumps stop abnormally, the PCS flow rate is decreased slowly by the pump flywheel in order to remove the decay heat.

Design point of the PCS pump is calculated based on the thermal design flow rate, uncertainty of the instruments and system resistance curve, aging effect of the plant and so on.

Thermal design flow rate is determined from the core thermal-hydraulic design. Thermal design flow rates for a research reactor which can be operating at both 3MW_{th} and 6MW_{th} are considered in this research. During the 3MW_{th} operation, PCS could be operated with the flow rate for the 6MW_{th}. But, PCS flow rate is reduced by the controller while the research reactor is in operation with the 3MW_{th} from the perspective of the plant aging effect and economy.

In this research, a required thermal design flow rate is assumed proportional to the reactor thermal power.

PCS pump type, NPSH margin and coastdown flow rate is designed and calculated in this research.

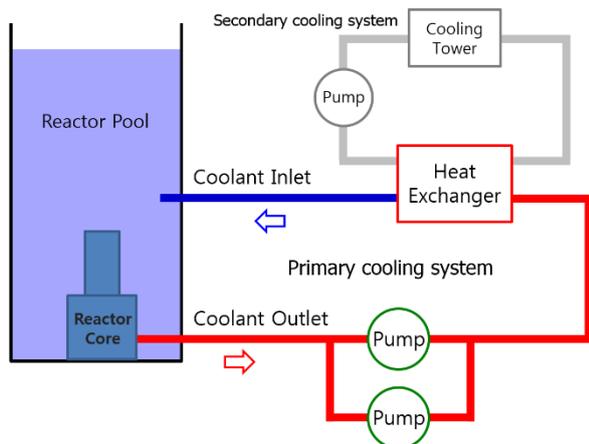


Figure 1. Schematic diagram of the primary cooling system.

2. PCS Pump Type

A centrifugal pump with a non-dimensional specific speed of 0.64 [-] and specific diameter of 4.64 [-] is conceptually considered as the PCS pump. Flow rate is adjusted by the change of the rotating speed of the impeller through the inverter control. Therefore, same pump can be used for the 3MW_{th} and 6MW_{th} operation. Pump is operated with the affinity laws as following.

Flow rate	$Q \propto \omega$
Head	$H \propto \omega^2$
Power	$P \propto \omega^3$

Pump design point of the flow rate and head is calculated based on the PCS flow band design. 109% of the thermal design flow rate is assumed as the PCS pump design flow rate in consideration of the thermal design flow, measurement uncertainty, plant aging effect and allowable flow band for start-up operation as shown in Fig. 2. Allowable flow band is calculated based on uncertainties of the system pressure drop characteristic, pump performance curve.

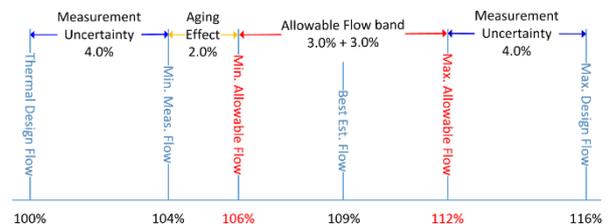


Figure 2. PCS flow band.

3. Cavitation

Cavitation is one of the most important factors to determine the stable operation of pump because cavitation makes the mechanical damage of the impeller, strong vibration and loud noise. In order to maintain the stable operation of the pump without cavitation at the impeller, the NPSH_A shall be larger than the NPSH_R. NPSH margin is generally expressed as a ratio of the NPSH_A and NPSH_R. This margin is determined by the working fluid, operation environment and user requirement. Generally, normal cold water has a margin of 130~150%. But, a pump used in the nuclear plant conservatively requires a margin of 150~250%.

Fig. 3 and 4 show the NPSH_A and NPSH_R coefficient of the PCS pump with the non-dimensional diameter of the pump inlet and capacity coefficient, respectively. These results are calculated from the 6MW_{th} operation.

$NPSH_R$ coefficient range from the minimum value to the maximum value is determined from the leading edge design of the impeller. Minimum $NPSH_R$ coefficient is required to secure the sufficient $NPSH$ margin. $NPSH_R$ is verified by the actual pump test.

When PCS pumps operate without cavitation at the flow rate for the $6MW_{th}$ operation, it can operate without cavitation at the $3MW_{th}$ operation. $NPSH_A$ coefficient is increased when the flow are is decreased as shown in Fig. 4. $NPSH_R$ is decreased when the rotating speed of the impeller is slowed down.

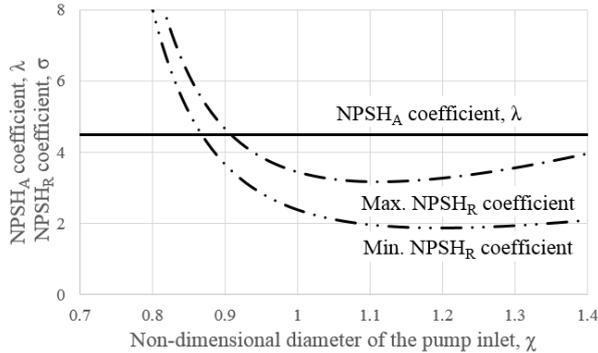


Figure 3. $NPSH_A$ and $NPSH_R$ coefficient with the non-dimensional diameter of the pump inlet

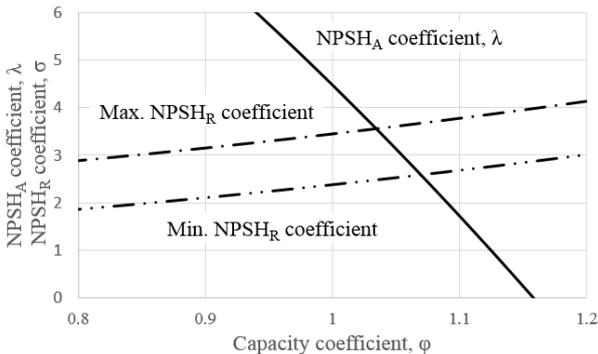


Figure 4. $NPSH_A$ and $NPSH_R$ coefficient with the capacity coefficient

4. Coastdown flow rate

Coastdown flow rate is calculated in consideration of the pump flywheel and linear momentum of the PCS.

In this study, a pump flywheel is designed to supply 80% of the normal core flow rate after 3sec from a pump stop.

Figure 5 shows the coastdown flow rate with the time. Coastdown flow rate satisfy the design requirement. Capacity coefficient at the $3MW_{th}$ operation is higher than that at the $6MW_{th}$ operation because of following relationships.

Flywheel Energy	$E_{flywheel} \propto \omega^2$
Fluid Kinetic Energy	$E_{fluid} \propto \omega^2$
Pump Power	$P \propto \omega^3$

Coastdown flow rate from the fluid kinetic energy is usually ignored for the conservative design.

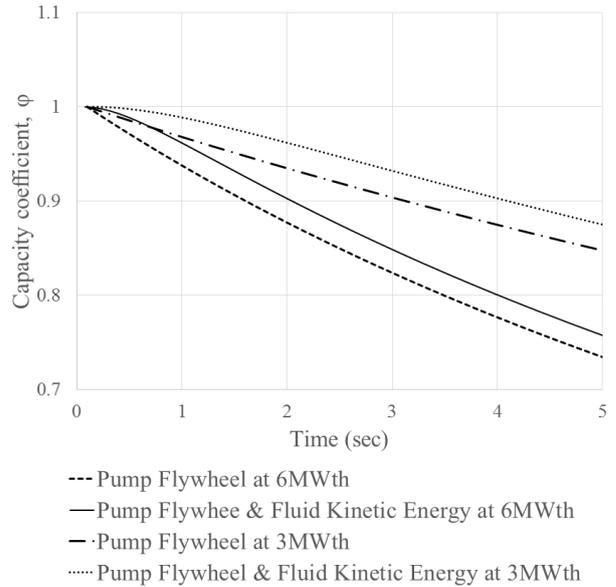


Figure 5. Coastdown flow rate with time

4. Conclusions

A centrifugal pump with a non-dimensional specific speed of 0.64 [-] and specific diameter of 4.64 [-] is conceptually designed in consideration of the $NPSH$ margin and required coastdown flow rate.

When the variable thermal design flow rate is required, the maximum required flow rate is the design point for the PCS pump and system design in consideration of the $NPSH$ margin and coastdown flow rate.

ACKNOWLEDGEMENT

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Nomenclature

d	Diameter of the impeller inlet, [m]
d ₁	Designed diameter of the impeller inlet, [m]
d _s	Specific diameter, $D \cdot (g \cdot H)^{0.25} / Q_d^{0.5}$, [-]
g	Acceleration of gravity, 9.81[m/s ²]
m	Mass of the fluid, [kg/s]
n _s	Specific speed, $\omega \cdot Q_d^{0.5} / (g \cdot H)^{0.75}$, [-]
u	fluid velocity in the pipe, [m/s]
D	Diameter of the impeller outlet, [m]
E _{fluid}	Fluid kinetic energy, $0.5 \cdot m \cdot u^2$, [J]
E _{flywheel}	Flywheel energy, $0.5 \cdot I \cdot \omega^2$, [J]
H	Pump Head at the design point, [m]
NPSH	Net Positive Suction Head, [m]
NPSH _A	Available NPSH, [m]
NPSH _R	Required NPSH, [m]
P	Pump power, [w]
Q	Flow rate, [m ³ /s]
Q _d	Flow rate at the design point, [m ³ /s]
V ₁	Velocity at the pump inlet, [m/s]
W _{th}	Thermal Power. [w]
λ	$NPSH_A \cdot g / V_1^2$, [-]
σ	$NPSH_R \cdot g / V_1^2$, [-]
φ	Q/Q _d , [-]
ψ	Pressure loss[m] · g/u ₁ , [-]
ω	angular velocity of the impeller, [rad/s]
χ	d/d ₁ , [-]