



**Modified Richardson number ( $Ri^*$ )**

$$Ri^* = \left( \frac{g \beta \Delta T_0 l_0}{u_0^2} \right) = \left( \frac{\text{Buoyancy}}{\text{Inertia}} \right) \quad (4)$$

**Modified Stanton number ( $St\#$ )**

$$St = \left( \frac{4hd_0 l_0}{(d_{cv}^2 - d_{sp}^2) \rho C_p u_0} \right) = \left( \frac{\text{Wall convection}}{\text{Axial convection}} \right) \quad (5)$$

**Friction number**

$$\sum_i \left( \frac{F_i}{A_i^2} \right) = \left( \frac{f_{l_0} + K}{d_0} \right) = \left( \frac{\text{Friction}}{\text{Inertia}} \right) \quad (6)$$

**2.2 Scaling analysis [4]**

Scaling analysis is performed to find the ratios of the variables between the prototype and model. The ratio between the model and prototype is denoted by R as following [5].

$$\Pi_R = \frac{\Pi_{\text{model}}}{\Pi_{\text{prototype}}} \quad (7)$$

Considering the space limitations that can be used for experiments while minimizing distortion, the model is selected to 3m height of the model and the heat flux ratio and the flow velocity ratio are also determined that 1.22 and 0.67 relatively (Table 1).

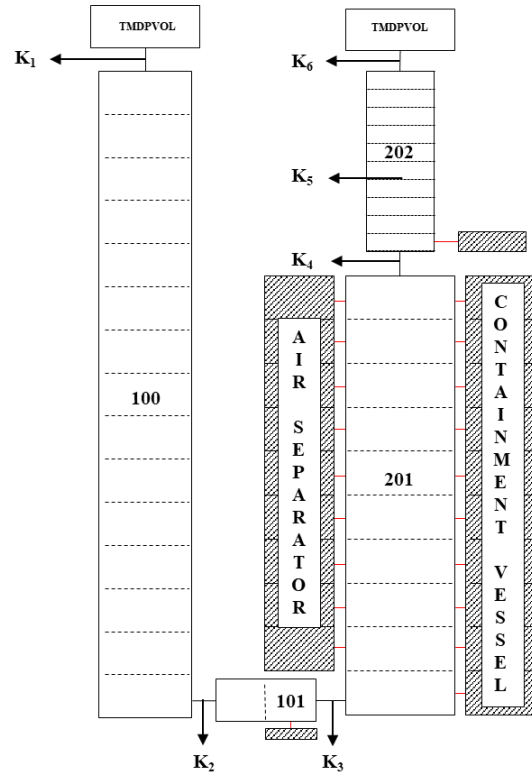
$l_R$	$l$ [m]	$d_R$	$d$ [m]	$u_R$	$q''_R$	$\Delta T_R$	$Ri\#_R$
0.10	0.67	0.56	0.17	0.32	1.78	1	1
0.30	2.01	0.74	0.22	0.55	1.35	1	1
0.45	3.00	0.82	0.25	0.67	1.22	1	1
0.60	4.02	0.88	0.26	0.77	1.14	1	1
0.75	5.03	0.93	0.28	0.87	1.07	1	1
0.90	6.03	0.97	0.29	0.95	1.03	1	1
1.00	6.70	1.00	0.30	1.00	1.00	1	1

**Table. 1 Different Models based on the scaling law**

**3. MARS-KS code simulation**

To evaluate the validity of the developed model, MARS-KS Code simulation is performed on the constant heat flux condition in the prototype and scale-down model. The MARS (Multi-dimensional analysis of reactor safety) code is the thermal-hydraulic system code for analysis of reactor transients. And, the heat removal performance also was compared with prototype and model. The air path modeled as a riser pipe (201) where the air is heated by convection in the CV and the SP and a down comer pipe (100) where the air flows, a horizontal pipe (101) connecting a down comer and a riser, a discharge pipe (202) were modeled in MARS-

KS. In case of discharge pipe, form loss coefficient can be set individually assuming that the damper is installed to satisfy Friction number similitude. To suppress the flow caused by the pressure head effect, the height of discharge and down comer was set to be same. Also, additional heat structure was set in the outlet of the horizontal pipe and the inlet of the discharge, and the radiation heat flux was calculated assuming that it was an enclosure (Fig. 2).



**Fig. 2. RVCS model in MARS-KS**

Assuming that the metal plate constituting the wall is polished well, the emissivity of the CV and SP wall are set by 1.5 and 2, respectively [6]. The form loss coefficient for the shape was determined by referring to the ASHRAE Handbook [7].

**3. Conclusions**

To assess the validity of the scaled model based on scaling analysis, it was compared the prescribed average velocity ratio ( $u_R=0.67$ ) and temperature difference ratio between outlet and inlet ( $\Delta T_R=1$ ) for the prototype and the scaled model with respect to the different form loss coefficient among scale down cases.

In Fig. 3, comparing the air temperature difference with the prototype and the scaled model, in the case of  $K=2.5$ , the temperature difference ratio related with the buoyancy effect is 1.004, which is most analogous to the prescribed temperature difference ratio ( $\Delta T_R=1$ ). In terms of the average velocity ratio related with inertia

effect, it was confirmed that the flow velocity ratio was 0.669 in the case of  $K=2.0$ , which is most analogous to the prescribed average velocity ratio ( $u_R=0.67$ )

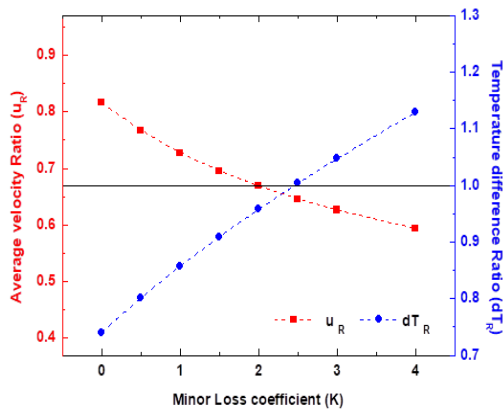


Fig. 3. Comparative Results of Average Velocity Ratio and Temperature Difference Ratio

The wall temperature of the CV and SP and the air temperature distribution are compared according to the height of prototype and scaled model ( $K = 2.0$ ). The air temperature and flow velocity can be predicted appropriately, but the temperatures of the CV and SP are slightly different. In fact, the scaled model requires higher heat fluxes condition ( $q''_R = 1.22$ ) and slower flow velocity ( $u_R = 0.67$ ), so the wall temperature of the scale model is higher (Fig. 3).

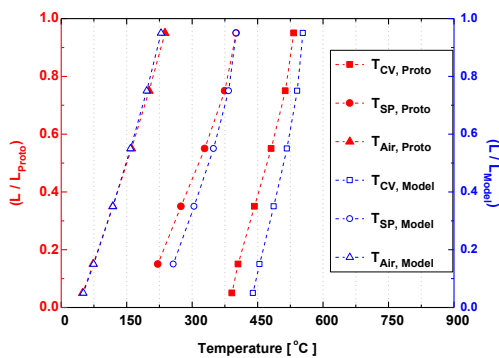


Fig. 3 Axial Temperature Distributions

To check the flow regime in the natural convection, the Rayleigh number ( $Ra_L$ ) of the prototype and scaled model were compared. It has been confirmed that both Prototype and scaled model exceeds critical Rayleigh number ( $\sim 10^9$ ), which is commonly known as the judgement criterion of turbulent flow on natural convection in vertical plate. Reynolds number ( $Re_D \#$ ) of the scaled model was slightly smaller than 2900, which is known as the fully turbulent region in pipe flow, but not significantly changed. Therefore, the validity of

the model developed through the scale analysis has been verified.

After all, a comprehensive assessment of the above results is that the  $K = 2.0$  model is best suited as a scaled model. Also, these results indicate that the proposed scaling analysis method predicts the RVCS cooling performance adequately and estimates the wall temperature slightly higher. This conservative evaluation ensures reliability of NPPs.

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