

Preliminary Simulation for Slug Flow Boiling on Downward Heated Surface

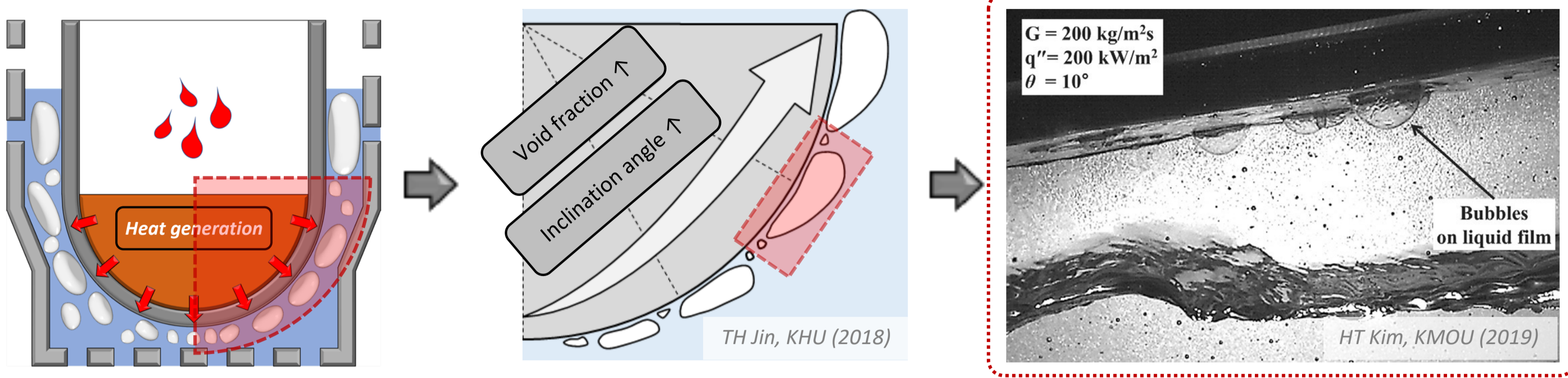
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Motivation and Objective

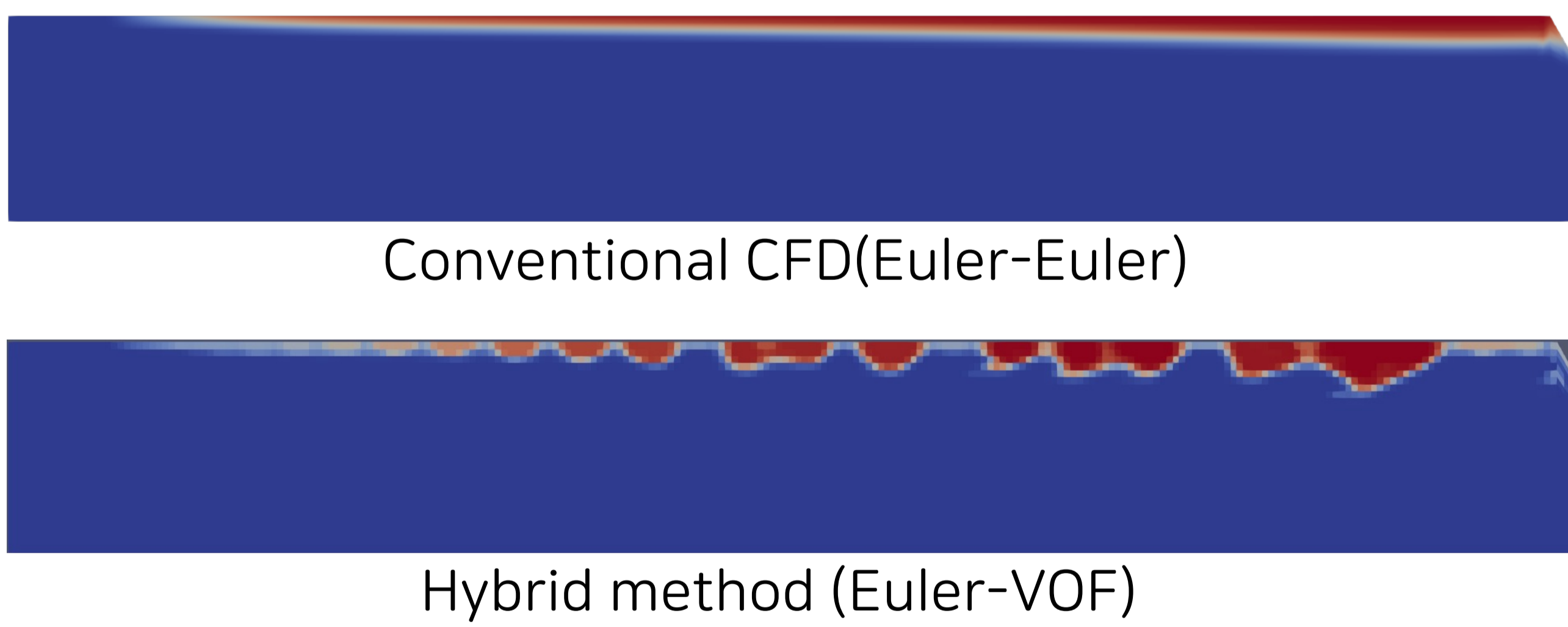


- IVR-ERVC has been presented in an effective way to maintain the integrity of reactor vessel during severe accident.
- The liquid film is formed beneath the slug bubbles and the heat conduction with high heat flux occurs due to this thin layer.
- However, the conventional wall boiling model of Kurul and Podowski does not properly simulate the heat transfer mechanism associated with liquid film of slug bubbles.
- To perform physics-based simulation of slug flow boiling, these two things are necessary.
 - To track the position of slug bubbles
 - To apply the wall boiling model considering the heat transfer through the liquid film

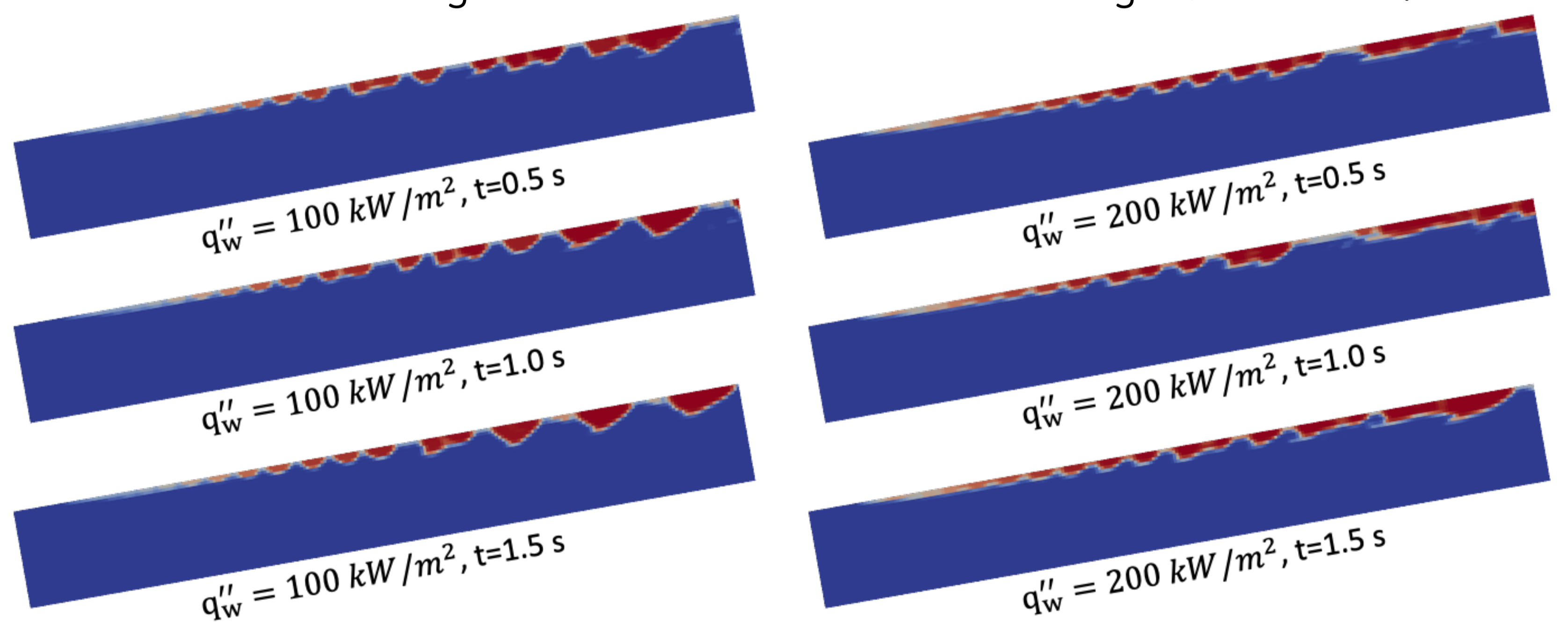
Objective: Development of a hybrid simulation methodology for flow boiling with dispersed and slug bubbles and conducting a preliminary simulation.

Simulation results

- Comparison with conventional CFD method
 - The result of conventional CFD method was similar to the film behavior.
 - Hybrid method simulated the distribution of bubbles more properly.



- Preliminary simulation for slug flow boiling on downward heated surface
 - The dispersed bubbles grew and the slug bubbles formed as merged.
 - The interfaces of slug bubble were well detected using VOF method.



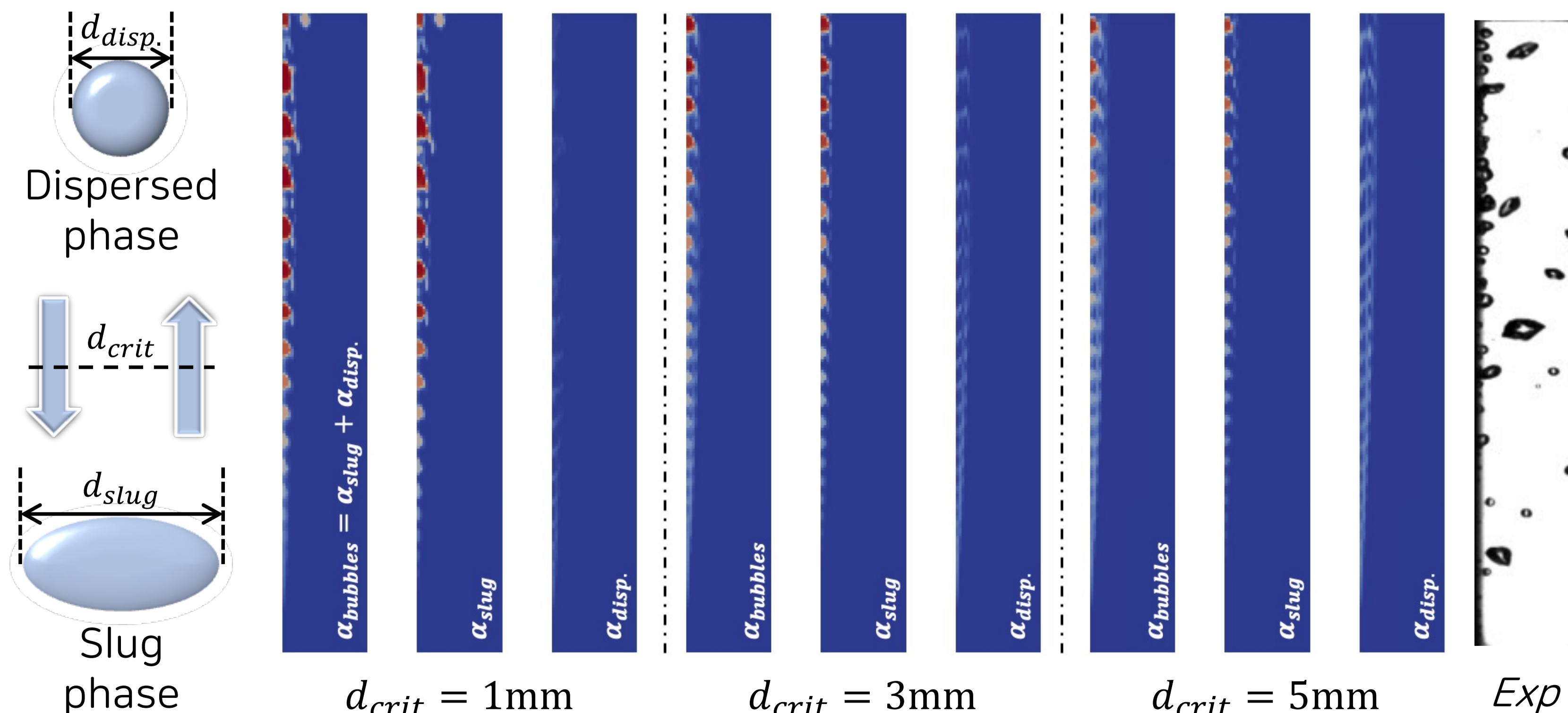
Conclusion & Future works

[Conclusion]

- The hybrid multiphase modelling which can tracking the position of slug bubble was developed.
- The wall boiling model was modified to consider heat transfer through the liquid film.
- The preliminary simulation of slug flow boiling on downward heated surfaces was conducted.

[Future works]

- The sensitivity test will be conducted to define the critical diameter for phase transfer
- The qualitative evaluation of WHFP model will be conducted using experimental data



[The effect of critical diameter on phase transfer]

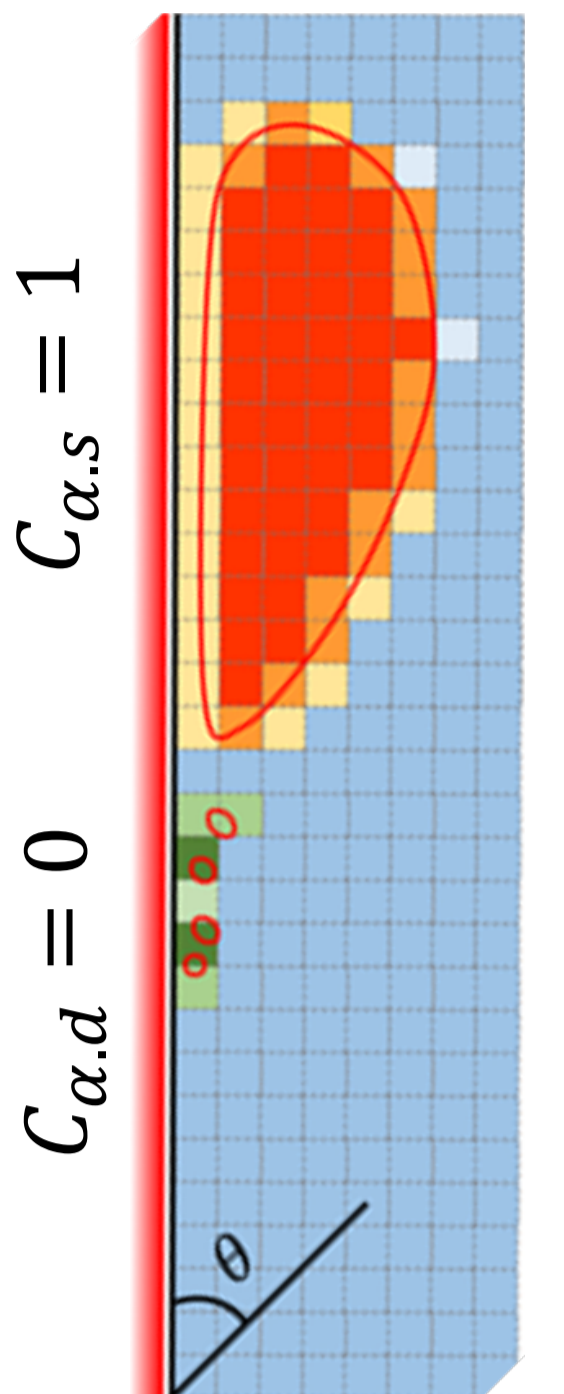
Simulation methods

Interface capturing method

- To track the position of slug bubbles, the hybrid multiphase solver was used which can apply the interface capturing method selectively between discrete and slug bubbles.

$$\frac{\partial \alpha_k}{\partial t} + \bar{u}_k \cdot \nabla \alpha_k + \nabla \cdot \left(C_{\alpha, phase} |\bar{u}| \frac{\nabla \alpha_k}{|\nabla \alpha_k|} (1 - \alpha_k) \right) = \frac{\Gamma_{ki} - \Gamma_{ik}}{\rho_k}$$

- $C_{\alpha, slug} = 1$ - Interface capturing on
- $C_{\alpha, dispersed} = 0$ - Interface capturing off



Hybrid Wall Heat Flux Partitioning (WHFP) model

- To track the position of s
- $q''_w = [1 - H(\alpha_{slug})] q''_{RPI} + H(\alpha_{slug}) q''_{slug}$
- Blending function for WHFP model

$$H(\alpha_{slug}) = \max \left(0, \min \left(1, \frac{\alpha_2^f - \alpha_{slug}}{\alpha_2^f - \alpha_1^f} \right) \right)$$

- WHFP model for continuous phase bubbles

$$q''_{slug} = \frac{k_l}{\delta_{film}} (T_w - T_{sat})$$

- WHFP model for dispersed phase bubbles

$$q''_{RPI} = q''_c + q''_q + q''_e \begin{cases} q''_c = h_c A_{1\phi} (T_w - T_l) \\ q''_q = h_q A_{2\phi} (T_w - T_l) \\ q''_e = N_a \left(\frac{\pi}{6} D_{dep}^3 \right) f \rho_g h_{fg} \end{cases}$$

