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Primary PFHE design for chloride based molten salt fast reactor



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Introduction	In this study, the offset strip fin			
■ The Molten Salt Reactor (MSR) is attracting global attention as a next-generation reactor due to its advantages such as inherent safety, high economy, and compact size.	type is used for PFHE, because it has a higher convective heat transfer coefficient compared to			
■ The Molten Salt Fast Reactor (MSFR) has the advantage of reducing waste disposal requirements by incinerating actinides from LWR used fuel.	other fin types.			
■ Since the chloride salt has a lower neutron absorption than the fluoride salt, making it more suitable for molten salt fast reactor with fast spectrum.	In a offset strip fins consist of fin gap (s), fin height (h), fin offset length (l), and fin thickness (t) as			
■ The conceptual design of an intermediate heat transport system for a chloride based molten salt fast reactor was carried out in this study.	shown in the right figure. The snape of the onset-strip in PFHE The ranges of heat exchanger design parameters are calculated by Korea Ator Example of the onset-strip in PFHE			

In previous study, the Plate Fin Heat Exchanger (PFHE) has a high potential as an intermediate heat transport system of MSR.

This study conducted a conceptual design of primary PFHE for MSR with working fluid as NaCl-MgCl₂



 \triangle The layout of MSR with power conversion system

Methods

■ The power conversion cycle for MSR is optimized using the KAIST-OCD code (Open Cycle Design).

■ The maximum temperature of a molten salt reactor is fixed in 650°C referring to the previous study.

The pinch temperature of intermediate heat exchanger is set to be 10K. Therefore, the turbine inlet temperature of the power conversion system is set to 630°C.

■ The air open Brayton cycle optimization design conditions and optimization results are as shown in below tables.

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\bigtriangledown Primary PFHE design pa	rameters range	
	Min.	Max.
Iot flow length [m]	0.1	2

Hot, Cold Fin height, h [m] 0.002 0.02 Fin thickness, t [m] 0.0001 0.0002 Hot, Cold Fin frequency, $1/n [m^{-1}]$ 0.001 0.015 Fin offset length, 1 (m) 0.001 0.015 Number of hot side layers 500 10 \blacksquare The thermal properties of coolant salt (NaCl-MgCl₂) are calculated as shown in below table. **▽** Thermal property and heat exchanger correlation for NaCl-MgCl₂

Thermal property

Heat capacity, $C_P = 1080.19 \left[\frac{J}{\text{kg} \cdot K} \right]$

Density, $\rho = (2297.1 - 0.507 \times T)$, for T < 973K

 $\rho = (2297.1 - 0.507 \times T), for T > 973K \left[\frac{\text{kg}}{m^3}\right]$

Dynamic viscosity, $\mu = \left(0.000286 \times exp\left(\frac{1441}{T}\right)\right) \left[\frac{\text{kg}}{m \cdot s} \right]$

Thermal conductivity, $k = 0.3133 + 0.000267 \times T \left| \frac{W}{m \cdot K} \right|$

■ The material properties of the fuel salt (NaCl-MgCl₂-[U-TRE-RE]Cl₃) required for the PFHE conceptual design were calculated by the radiochemical laboratory

\bigtriangledown (Cycle	optimi	zation	parameters	and	results
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Cycle optimization parameters ((Fixed variable)	Cycle optimization results		
Air intake temperature [°C]/ Humidity	40 / Dry	Cycle optimization resul		
Max temperature [°C]	630 Cycle thermal efficiency [%]		32.01	
Thermal heat [MWth]	6.5	6.5 Cycle net work [MWe]		
Compressor inlet pressure [kPa]	101.325	Succific weat [NAV//Iro]	0.001	
Turbine efficiency	90	Specific work [IVI we/kg]	0.0814	
Compressor efficiency [%]	86	Thermal heat [MWth]	6.5	
Recuperator effectiveness [%]	92			
Component pressure dr	op ratio	Pressure ratio		
Heater Cold side	0.02	Max. Pressure [MPa]	0 347	
Recuperator Hot side	0.01		0.517	
Recuperator Cold side	0.01	Mass flow rate of NaCl-MgCl ₂ (kg/s)	25.55	
Ratio of exhaust pressure to The thermapsizing of the MSR ^{0.98} system is performed as follows.				

■ The minimum temperature of NaCl-MgCl₂ in the heat exchanger is set to 550°

in KAERI.

▽ Material properties of the fuel salt (NaCl-MgCl₂-[U-TRE-RE]Cl₃)

Salt	Temperature	Heat Capacity [J/kg·K]		Viscosity [cP]	Thermal Conductivity [W/m·K]	
Salt [°C]		Mole fraction additive method		Mole fraction additive method	Igatieve and Khoklove correlation	
	550	688.183		2.646	0.333	
NaCl-MgCl ₂ -	600	694.833		2.232	0.358	
(U-TRE-RE)Cl ₃	650	701.791		1.918	0.383	
	700	709.055		1.674	0.408	
Result						
The conceptual design results of the primary PFHE are summarized as follows.						
	\bigtriangledown MS	SR primary PFHE	conc	eptual design results		
Hot Fin he	ight [m]	0.002		umber of hot side layers	80	
Cold Fin he	n height [m] 0.002		Number of cold side layers		81	
Fin thickn	Fin thickness [m] 0.00011		HX width [m]		0.5	
Hot Fin freque	quency $[m^{-1}]$ 1000		HX length [m]		2.56	
Cold Fin frequ	ency [m ⁻¹]	/ [m ⁻¹] 1000		HX height [m]	0.40	
Fin offset le	ngth [m]	[m] 0.003		Plate thickness [m]	0.0005	
Hot side pressur	ot side pressure drop [kPa] 167		Volume core [m ³]		0.51	
Cold side pressure drop [kPa] 108 Heat transfer effectiveness [%] 92.19 The structural material for the primary PFHE is selected as SS316 (SA-213) TP316H) which can operate at maximum temperature of 800 °C						
Conclusions						
■ In this study, the primary PFHE of a molten chloride salt fast reactor is conceptually designed.						
■ The chloride salt is used as a working fluid in this study because chloride salts have lower neutron moderating capability for molten salt fast reactor.						
■ Using the optimization and thermal sizing results, the conceptual design of primary PFHE using fuel salt (NaCl-MgCl ₂ -TRUCl ₃) and coolant salt (NaCl-MgCl ₂) is performed in this study.						

to avoid freezing risk.

• The mass flow rate of the primary PFHE that can simultaneously satisfy th maximum temperature and the pinch temperature of 10K condition was calculated. \bigtriangledown MSR Primary PFHE thermal sizing results

$\Delta T_{hot \ side \ inlet-cold \ side \ inlet}$ [K]	10		
Primary PFHE hot side			
Mass flow rate [kg/s]	100.38		
Inlet temperature [°C]	650		
Outlet temperature [°C]	560		
Primary PFHE cold side			
Mass flow rate [kg/s]	65.21		
Inlet temperature [°C]	550		
Outlet temperature [°C]	640		