Numerical study on the design parameters of a packed bed thermal energy storage system

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Introduction

- Renewable energy generation rate \uparrow , intermittency issue arises
- Thermal energy storage (TES) can be a key solution for grid stability problem
- TES is considered for flexible operation of NPPs





TES system using packed bed

- Thermocline thermal energy storage (TES)
 - ✓ Charging: hot fluid in \rightarrow cold fluid out
 - ✓ Discharging: cold fluid in \rightarrow hot fluid out
- Hot and cold fluid is separated by thermal stratification
 - ✓ Thermocline formation
- Packed bed thermal energy storage
 - ✓ Randomly packed solid filler in cylindrical tank
 - \checkmark Heat storage through convective heat transfer
 - ✓ Cost effective



Principle scheme of packed bed TES [Baeuerle, 2017]

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Object of present study

- Parametric study of packed bed TES using numerical analysis
 - ✓ Numerical evaluation of thermal performance varying design parameter
 - Flow velocity (*u*) I.
 - II. Tank height (H)
 - III. Porosity (ε)
 - IV. Heat transfer fluid
- Provide basic data for packed bed TES system design



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Model description



Parameters of packed bed TES



Design parameters			
Parameters	Values		
Hear transfer fluid	Molten salt		
Solid filler	Quartzite rock		
Tank height [m]	6		
Tank diameter [m]	3		
Filer diameter [m]	0.01905		
Initial hot temperature [K]	663.15		
Initial cold temperature [K]	563.15		
Flow velocity [m/s]	0.001		
Porosity	0.22		

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- In this work, the discharging process was simulated and analyzed
- Distributors are installed near the tank's inlet and outlet to ensure uniform flow distribution



Parametric study

Test matrix of packed bed TES

Parameters	Values	
Flow velocity [m/s]	5×10 ⁻⁴ -3×10 ⁻³	
Tank height [m]	2–8	
Porosity	0.12–0.42	
	Molten salt	
Heat transfer fluid	Therminol-66	
	Liquid sodium	

- Varied parameters
 - I. Flow velocity (*u*)
 - II. Tank height (*H*)
 - III. Porosity (ϵ)
 - IV. Heat transfer fluid



Numerical method

- Simulation was performed by adopting the CFD code based on ANSYS Fluent
- Three-dimensional flow was simulated in transient mode
- Assumptions
 - I. Uniform flow of constant velocity is injected into the tank
 - II. Flow motion is laminar
 - III. Packed bed region is insulated (adiabatic condition)
 - IV. The properties of working fluid and solid filler are independent of temperature
- PISO algorithm is used for the pressure-velocity coupling
- Time step size is 1 s and residual is 10⁻⁴



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Sensitivity analysis



- Since the case for 5.56×10^5 , the maximum relative error has decreased by 0.8 %
- The case for 1.04×10^6 , was adopted in consideration of the error rate and calculation time



Thermal performance indicator

• Thermocline thickness



• Energy efficiency

$$\eta = \frac{\int_{0}^{t_{dischar.}} \dot{m} \ C_{p,f} [T_{f,out}(t) - T_{cold}] dt}{\int_{0}^{t_{char.}} \dot{m} \ C_{p,f} [T_{hot} - T_{cold}] dt}$$
(3)

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Results and discussion



Validation



- The numerical results were compared with the results of existing study
 - ✓ Average relative error = 2.1 %



Influence of flow velocity



Flow velocity [m/s]	Thermocline thickness [m]	Discharging time [h]	Energy efficiency
5×10 ⁻⁴	0.354	0.28	0.748
1×10 ⁻³	0.152	0.47	0.840
2×10 ⁻³	0.120	0.64	0.869
3×10-3	0.105	0.81	0.884

Results of study for flow velocity

H = 6 m, $\varepsilon = 0.22$, molten salt, discharging mode

- $u \uparrow$, thermocline thickness \downarrow , Efficiency \uparrow
 - \checkmark Heat transfer between the fluid and the solid filler was improved
 - \checkmark Residence time of the thermocline within the tank was shortened



Influence of tank height



Results of study for tank height			
Tank height [m]	Normalized thermocline thickness	Discharging time [h]	Energy efficiency
2	0.354	0.28	0.748
4	0.152	0.47	0.840
6	0.120	0.64	0.869
8	0.105	0.81	0.884

$u = 3 \times 10^{-3}$ m/s, $\varepsilon = 0.22$, molten salt, discharging mode

- Thermocline thickness normalized according to tank height
- $H\uparrow$, thermocline thickness \uparrow
 - \checkmark Expansion time of thermocline has increased
- $H\uparrow$, normalized thermocline thickness \downarrow , Efficiency \uparrow
 - ✓ Increase in storage capacity had a greater impact on efficiency





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Influence of porosity



Results of study for porosity			
Porosity	Thermocline thickness [m]	Discharging time [h]	Energy efficiency
0.12	0.826	2.17	0.807
0.22	1.062	2.25	0.804
0.32	1.181	2.33	0.801
0.42	1.298	2.42	0.798

Results of study for porosity

$u = 3 \times 10^{-3}$ m/s, H = 6 m, molten salt, discharging mode

- $\varepsilon \uparrow$, thermocline thickness \uparrow
 - Reduced the heat transfer area of the solid filler and impaired the heat transfer between the fluid and solid filler
- Energy efficiency was similar in the all cases for porosity
 - \checkmark Area of the fluid by the porosity compensated for this



Influence of heat transfer fluid



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Heat transfer fluid	Thermocline thickness [m]	Discharging time [h]	Energy efficiency
Molten salt	1.179	2.25	0.796
Therminol-66	1.184	2.86	0.840
Liquid sodium	1.298	3.97	0.775

Results of study for HTF

 $u = 3 \times 10^{-3}$ m/s, H = 6 m, $\varepsilon = 0.22$, discharging mode

- Molten salt showed the smallest thermocline thickness
- Therminol-66 showed the best energy efficiency
- Liquid sodium is bad for packed bed TES system
 - \checkmark Low energy efficiency, long discharging time, high thermal conductivity



Conclusions and further studies

Conclusions

- Packed bed TES was simulated using numerical method and verified compared to results of existing study
- The influence of design parameters on packed bed TES was conducted
 - ✓ u ↑, thermocline thickness ↓, Efficiency ↑
 - ✓ H ↑, normalized thermocline thickness ↓, Efficiency ↑
 - ✓ ε ↑, thermocline thickness ↑

Further studies

- Parametric study for added the deign parameters
- Improved model for NPP system
- Effect of distributor on thermocline in TES



Thank you for attention.

