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## Layout of presentation



- > Introduction (why ettringite &  $^{14}C$ ?)
- Synthesis & characterization of ettringite
- Application of ettringite for sequestration of <sup>12</sup>C (non-radioactive surrogate of <sup>14</sup>C) from simulated waste solutions (NaHCO<sub>3</sub>)

 $As HCO_3^-$  (at intermediate pH ~8.50)

• As  $CO_3^{2-}$  (at high pH ~11.50)

- Desorption tests
- Conclusions



## Why ettringite &<sup>14</sup>C?



- > Carbon-14 (<sup>14</sup>C), a radionuclide generated in nuclear power plants and nuclear reactor operation, is a serious environmental threat due to its long half-life ( $t_{1/2} = 5730$  years) and potential mobility in the environment.
- A large quantity of <sup>14</sup>C is being produced in the reactor water (coolant and moderator), can be discharged from the nuclear facilities into rivers and/or seas and enhance the concentration of <sup>14</sup>C in the aqueous environment.
- > Depending on the pH of the solution, the dissolved inorganic carbon can be distributed carbon dioxide ( $CO_2(aq)$ ), bicarbonate ( $HCO_3^-$ ), and carbonate ion ( $CO_3^{2-}$ ).
- In alkaline aqueous media/waste solution, <sup>14</sup>C mainly exists as dissolved inorganic carbonate species (bicarbonate and carbonate).





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- Ettringite is a hydrous calcium aluminum sulfate naturally occurring mineral and a hydration product of Portland cement [Ca<sub>6</sub>Al<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub>(OH)<sub>12</sub>·26H<sub>2</sub>O].
- J. Lehmann (in 1874) coined the term ettringite due to it occurrence near the Ettringer Volcano, Ettringen, Germany.
- It is known to immobilize anions via substituting a) TcO<sub>4</sub><sup>-</sup> and IO<sub>3</sub><sup>-</sup> for sulfate (SO<sub>4</sub><sup>2-</sup>)) from the channels as well as b) AsO<sub>4</sub><sup>3-</sup>and SeO<sub>3</sub><sup>2-</sup> for OH or H<sub>2</sub>O from ettringite surface (≡Ca-OH<sub>2</sub>, ≡AI-OH) or channel (≡Ca-OH<sub>2</sub>) sites.





## **Synthesis of ettringite**



**Reagents/Chemicals:** Calcium nitrate tetrahydrate  $[Ca(NO_3)_2.4H_2O]$ , aluminum sulfate octadecahydrate  $[AI_2(SO)_3.18H_2O]$ , sodium hydroxide (NaOH), and deionized water (DIW).





#### Characterization of synthesized ettringite



**Figure 1.** Characteristics of synthesized ettringite. (a) Wide-angle X-ray diffraction (XRD) pattern of material with major reflections at their corresponding 20 values. (b) N<sub>2</sub> adsorption/desorption isotherms and BJH pore size distribution (inset Figure) data. (c) The FT-IR spectrum. (d) FE-SEM image.



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### Sequestration of HCO<sub>3</sub><sup>-/</sup>CO<sub>3</sub><sup>2-</sup> from simulated waste solutions

- Experiments were performed in polypropylene tubes (PPT) using simulated waste solutions (100 ppm NaHCO<sub>3</sub> in DIW; except the change in conc. of simulated waste samples).
  - I. At intermediate pH (8.50), the existing species will be  $HCO_3^-$
  - II. Whereas,  $CO_3^{2-}$  species will dominate at high pH (11.50)
- Solid to waste solution ratio = 2 g/L and the samples were kept under dynamic condition using benchtop shaker (speed: 150 rpm) at RT.
- Various parameters, including contact times (kinetics) and concentrations of solid/ettringite and waste solutions were varied.
- Reaction time:10 m, 30 m, 1 h, 2 h, 4 h, 8 h, 12 h, 24 h, 48 h, 60 h, and 72 h.
- Pseudo first and second order kinetic modelling.
- Initial concentrations of HCO<sub>3</sub><sup>-</sup> and CO<sub>3</sub><sup>2-</sup> anions were varied as 36 ppm, 72 ppm, 108 ppm, 144 ppm, 180 ppm, and 216 ppm.
- Freundlich sorption isotherm analysis.



## Sequestration of CO32- from simulated wastes of 바라궁원자력학호



**Figure 2.** Sequestration of  $CO_3^{2-}$  anions simulated waste solution using from ettringite at high pH (~11.50) condition. (a) Kinetics of CO32- anions removal [CO32anions = 72 ppm; S/L = 2 g/L; contact time = 5 m - 60 h] (b) Pseudo-first-order kinetic model for removal of  $CO_3^{2-}$  anions. (c) Applicability of pseudo-second-order kinetic model for removal of  $CO_3^{2-}$  anions. (d) Effect of initial CO<sub>3</sub><sup>2-</sup> concentration in waste solution  $[CO_3^{2-} anions = 36 ppm - 216 ppm;$ S/L = 2 g/L; contact time = 8 h]. (e) Freundlich sorption isotherm analysis for removal of  $CO_3^{2-}$  anions. (f) Effect of sorbent concentration on CO32- removal  $[CO_3^2 \text{ anions} = 72 \text{ ppm}; \text{ S/L} = 0.5 \text{ g/L} - 4.0$ q/L; contact time =8 h].

![](_page_7_Picture_3.jpeg)

#### **Mechanism of CO<sub>3</sub><sup>2-</sup> anions sequestration using ettringite**

![](_page_8_Figure_1.jpeg)

### Sequestration of HCO<sub>3</sub><sup>-</sup> from simulated waste solution

![](_page_9_Figure_1.jpeg)

Figure 4. Sequestration of HCO<sub>3</sub>anions using ettringite from simulated waste solution at intermediate pH (~8.50). (a) Kinetics of  $HCO_3^-$  anions removal [HCO<sub>3</sub><sup>-</sup> anions = 72 ppm; S/L = 2 g/L; contact time = 10 m - 72 h] (b) Pseudo-first-order kinetic model for removal of  $HCO_3^-$  anions. (c) Pseudosecond-order kinetic model for sequestration of  $HCO_3^-$  anions. (d) Effect of initial HCO<sub>3</sub><sup>-</sup> concentration in waste solution  $[HCO_3^- \text{ anions} = 36]$ ppm -216 ppm; S/L = 2 g/L; contact time = 48 h]. (e) Effect of sorbent concentration on HCO<sub>3</sub><sup>-</sup> removal  $[HCO_3^- anions = 72 \text{ ppm}; \text{ S/L} = 0.5 \text{ g/L}$ -3.0 g/L; contact time = 48 h].

![](_page_9_Picture_3.jpeg)

#### Mechanism of HCO<sub>3</sub><sup>-</sup> anions sequestration using ettringite

![](_page_10_Figure_1.jpeg)

prior (black data) and after removal of HCO<sub>3</sub>anions (colored curves) at 36 ppm-216 ppm initial HCO<sub>3</sub><sup>-</sup> concentrations in simulated waste solutions at intermediate pH (8.50). (b) The combined FT-IR spectra of ettringite (black) and after removal of HCO<sub>3</sub><sup>-</sup> anions (colored data) at different initial  $HCO_3^{-1}$  anions <sup>500</sup> concentrations. (c) The FE-SEM image and

| EDS elemental manning of synthesized                        |  |                   |
|---|--|-------------------|
| /pes of<br>orbent   | Initial concentration of anions in sequestration experiments | S content (Wt. %) |
| ynthesized<br>tringite                                      | NIL  | 6.84              |
| ttringite<br>ter removal<br><sup>•</sup> HCO <sub>3</sub> - | 72 ppm initial concentration of $HCO_3^-$                    | 2.43              |
|   | 216 ppm initial concentration of $HCO_3^-$                   | 0.95              |

#### waste solutions.

| Wavenumber (cm <sup>-1</sup> ) | Assignment     |  |
|--------------------------------|----------------|--|
| 1418                           | C-O stretching |  |
| 1668                           | O-H bending    |  |
| 1110                           | S-O stretching |  |
| 850                            | AI-O-H bending |  |

#### **Desorption tests**

![](_page_11_Picture_1.jpeg)

- > Desorption behavior of  $CO_3^{2-}$  and  $HCO_3^{-}$  anions from ettringite in simulated groundwater (SGW).
- Two sets of desorption experiments were performed in SGW condition both at its natural pH (~ 9.00) and adjusted pH (~ 11.50).
- > SGW = 100 ppm NaNO<sub>3</sub>, 100 ppm KCI, 100 ppm Na<sub>2</sub>SO<sub>4</sub>, and 50 ppm Na<sub>3</sub>PO<sub>4</sub> in DIW
- > Solid to solution ratio (ettringite to DIW) = 2g/L; Contact time 1 to 7 days.
- Samples were tested under dynamic condition using benchtop shaker (speed: 150 rpm) at RT.
- > Desorption data were calculated in terms of desorption (%) and retention capacity (%).

![](_page_11_Figure_8.jpeg)

![](_page_11_Picture_9.jpeg)

![](_page_12_Picture_0.jpeg)

![](_page_12_Picture_1.jpeg)

- Characterization results (XRD, SEM, and FT-IR) confirmed the <u>synthesis of highly</u> <u>crystalline homogeneous ettringite.</u>
- Synthesized ettringite was used for the sequestration of carbonate anions both at intermediate and high pH conditions at RT.
- Obtained results revealed ~ <u>92-94 % sequestration of <sup>12</sup>C (surrogate of <sup>14</sup>C) from simulated waste solutions onto ettringite was achieved in 48 h and 8h at intermediate pH (~8.5) and high pH (~11.50), respectively.</u>
- FESEM-EDS analysis and XRD results indicated a considerable phase alteration of ettringite at intermediate pH (HCO<sub>3</sub><sup>-</sup>) removal tests. However, <u>the ettringite structure was</u> <u>quite stable at high pH (CO<sub>3</sub><sup>2-</sup>) removal experiments.</u>
- Pseudo second order kinetic and Freundlich isotherm model was applied for the removal of carbonate anions onto ettringite.
- Ettringite demonstrated efficient  $CO_3^{2-}$  and  $HCO_3^{-}$  sequestration from simulated waste solution via ligand exchange, substituting  $OH/H_2O$  and  $SO_4^{2-}$  species from ettringite, respectively.
- Desorption results (retention capacity) suggested that the synthesized ettringite can be potentially applied for removal of <sup>14</sup>C from waste solutions both at the intermediate and high pH conditions.

Korea Atomic Energy Society 2024 Spring Academic Conference (May 8-10)

![](_page_13_Picture_1.jpeg)

# I sincerely appreciate your attention

## Any Questions ?

![](_page_13_Picture_4.jpeg)